

Comparison of Turbulence Models for an Internal Flow with Side Wall Mass Injection

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Introduction

Solid propellant rocket boosters (SPRB) are used extensively in aerospace activities when a strong thrust is needed as in the case of lifting off the satellites for space activities [1]. Flow structures occurring within the SPRB's have drawn the attention of the researchers either experimentally [2,3], or as it happens increasingly today, computationally [4,5]. The flow field inside the combustion chamber experiences different processes since the characteristic velocity throughout the chamber is on the order of $Ma = O(10^{-2})$ [6], whereas the exit velocity is supersonic. Time dependent behavior of various processes, turbulence, combustion, as well as with the compressibility effects add intricacy into the simulation processes. Today, major study field for the SPRBs is the flow stability problem inside the combustion chamber [6], and its interaction with combustion [7] and turbulence [8].

This study is the first part of an ongoing research held in the Faculty of Mechanical Engineering at Istanbul Technical University (ITU), to simulate the interaction of the turbulence, combustion and the acoustic field inside SPRBs. In this preliminary work, a computational study has been performed to identify the effect of various turbulence models on the calculations of cold flow field inside a model SPRB combustion chamber. A commercial flow solver, Fluent 6.1.22, has been employed for the computations.

The flow configuration chosen is an idealization of that found in a solid rocket motor, and was selected in accordance with the VECLA facility of ONERA that is an experimental set up for investigating the characteristics of injection driven flows [4,8,9]. Schematic of the facility is given in Figure 1, where the length of the channel is $L = 0.581$ m and its height is $h = 0.0103$ m. The channel is bounded at $y/h = 0$ by a permeable wall allowing the mass injection and at $y/h = 1$ by an impermeable wall. The upstream at $x/L = 0$, head-end, is closed and the downstream, at $x/L = 1$, exit section, is open to the atmosphere. Sidewall mass injection is used to mimic the normal velocity of gaseous products generated by combustion of gasified propellant.

For this particular work, based on the Reynolds averaged Navier Stokes equations, computations have been performed by modeling the turbulence with one equation model (Spallart Allmaras), two equation models (Standard $k-\epsilon$, RNG $k-\epsilon$, Realizable $k-\epsilon$, SST $k-\omega$) and the Reynolds Stress model. Set of governing equations has been solved by employing the Finite Volume technique [10]. Boundary conditions were specified as, air injection mass flux, $\dot{m} = 2.619$ kg/m²s, and the appropriate turbulence quantities, $\tilde{k} = 0.0001$ m²/s², $\tilde{\epsilon} = 0.001$ m²/s³, $\tilde{\omega} = 0.4$ 1/s, at the permeable wall; pressure outlet, 137400 Pa, in the exit section and no slip condition for the impermeable wall at $y/h = 1$ and the solid wall in the head-end, at $y/h = 0$. Reynolds number based on the injection velocity and the channel height, Re_i , is approximately 8000. Density was calculated by the ideal gas law, and hence air injection temperature, 300 K, was specified. Normalized longitudinal velocity and the turbulent intensity profiles calculated with various turbulence closure models are compared with those from the experiment reported in [9] at several cross sections.

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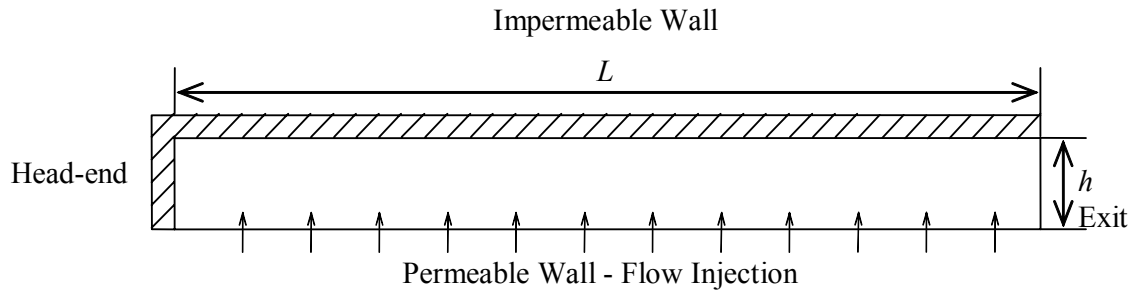


Figure 1. Schematic of computational domain

Results and Discussion

The injection Reynolds number was chosen as to produce a statistically stationary flow field and the first set of computations dealt with the comparison of the longitudinal velocity profiles obtained by steady and time marching feature of the FLUENT. It was shown that the profiles match excellently, allowing us to exploit the steady solver. In the next step, several turbulence closure models have been employed for computations and the calculated longitudinal velocity and turbulence intensity profiles were compared with those obtained from an experimental study reported by [9]. It is seen from Figure 2 that, Spalart-Allmaras turbulence closure model failed to compute satisfactory results. Computations based on the Reynolds stress model predicted the normalized longitudinal velocity profiles in a good agreement with the experiments. However, some discrepancy is detected in the neighborhood of the impermeable wall, hence; the validity of the closure model is questionable in this region. It was possible to acquire the longitudinal velocity profiles in the entire channel with a good accuracy with the SST $k-\omega$ model.

As given in Figure 3, the turbulence intensity levels obtained with the standard $k-\epsilon$ model failed to capture the experimental profiles. However, the turbulence intensity profiles obtained with the SST $k-\omega$ model are satisfactory, except for the second peak observed in the close neighborhood of the upper impermeable wall. Indeed, the accuracy of the experiment can be questionable in this region [9] because the existence of an impermeable wall may be expected to increase the turbulence levels in this region, leading to a possible peak.

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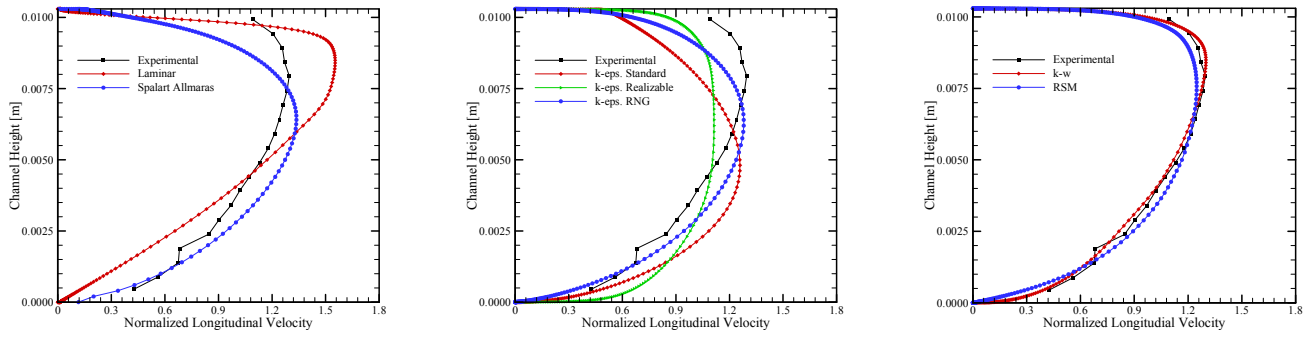


Figure 2. Normalized longitudinal velocity profiles, at $x = 0.500$ m, obtained with a) Laminar and Spalart-Allmaras, b) Standard $k-\epsilon$, RNG $k-\epsilon$ and Realizable $k-\epsilon$, c) Reynolds stress and SST $k-\omega$ closure models and from the experiment [9].

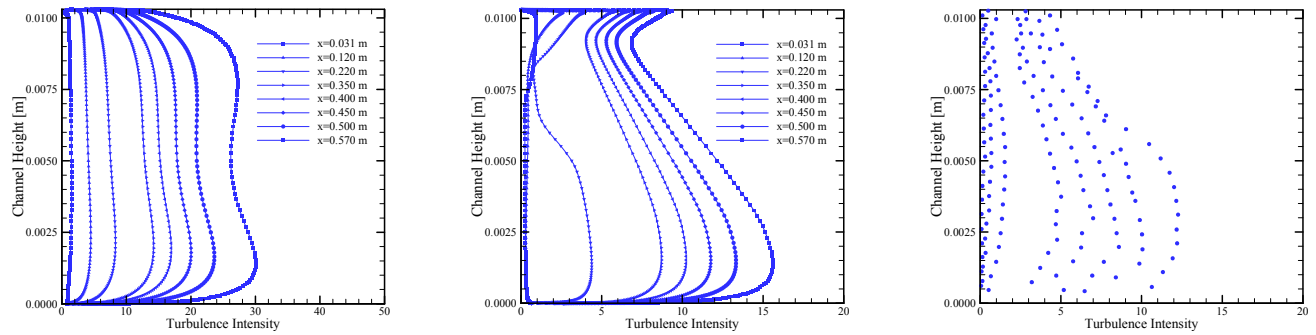


Figure 3. Turbulence intensity profiles obtained with a) Standard $k-\epsilon$, b) SST $k-\omega$ and from c) Experiment [9].

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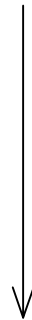


- Introduction
- Governing Equations
- Numerical Models and Boundary Conditions
- Computational Results
- Conclusion



Major Mechanisms in SPRB Flow Evolution

- Local flow oscillations
- Combustion instability
- Acoustic disturbances



Flow Instability

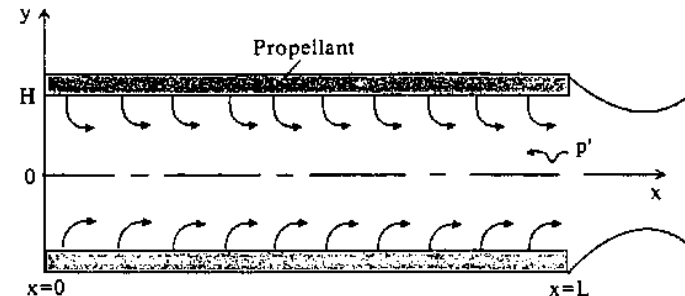


Figure 1. Schematic of a SPRB

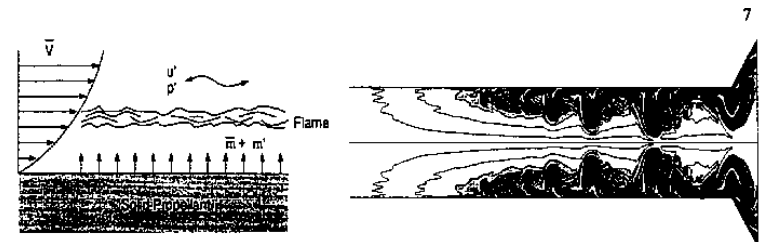


Figure 2. Unsteady flow evolution inside a SPRB

(V., Yang *et.al.* 1992-2004)

(Kirkkopru, K., Kassoy, D. R., 1996-2002)



Experimental Studies

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2003. |
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Reynolds Average

$$\overline{\Phi}(x, t) = \Phi(x, t) + \Phi'(x, t)$$

$$\Phi(x, t) = \lim_{T \rightarrow \infty} \frac{1}{T} \int_t^{t+T} \Phi(x, t) dt$$

Favre (Mass) Average

$$\Phi_i = \tilde{\Phi}_i + \Phi_i''$$

$$\tilde{\Phi} = \frac{1}{\bar{\rho}} \lim_{T \rightarrow \infty} \frac{1}{T} \int_t^{t+T} \rho(x, \tau) \Phi(x, \tau) d\tau$$

$$\tilde{\Phi}(x, t) = \overline{\rho \Phi(x, t)} / \bar{\rho}$$



Continuity

$$\frac{\partial \bar{\rho}}{\partial t} + \frac{\partial}{\partial x_i} (\bar{\rho} \tilde{u}_i) = 0$$

Momentum

$$\frac{\partial}{\partial t} (\bar{\rho} \tilde{u}_i) + \frac{\partial}{\partial x_j} (\bar{\rho} \tilde{u}_j \tilde{u}_i) = -\frac{\partial P}{\partial x_i} + \frac{\partial}{\partial x_j} [\bar{t}_{ji} - \overline{\rho u_j'' u_i''}]$$

Energy

$$\begin{aligned} \frac{\partial}{\partial t} \left[\bar{\rho} \left(\bar{e} + \frac{\tilde{u}_i \tilde{u}_i}{2} \right) + \frac{\overline{\rho u_i'' u_i''}}{2} \right] + \frac{\partial}{\partial x_j} \left[\bar{\rho} \tilde{u}_j \left(\bar{h} + \frac{\tilde{u}_i \tilde{u}_i}{2} \right) + \tilde{u}_j \frac{\overline{\rho u_i'' u_i''}}{2} \right] \\ = \frac{\partial}{\partial x_j} \left[-q_{Lj} - \overline{\rho u_i'' h''} + \bar{t}_{ij} u_i'' - \overline{\rho u_j'' \frac{1}{2} u_i'' u_i''} \right] + \frac{\partial}{\partial x_j} \left[\tilde{u}_i (\bar{t}_{ij} - \overline{\rho u_j'' u_i''}) \right] \end{aligned}$$

State Equation(Perfect Gas)

$$P = \bar{\rho} R \tilde{T}$$



First Order Models

- Spalart Allmaras Model
- Standard k - ε model
- RNG k - ε model
- Realizable k - ε model
- SST k - ω model

Boussinesq approximation

$$-\overline{\rho u_j'' u_i''} = 2\mu_T \tilde{S}_{ji} - \left(\frac{2\mu_T}{3} \right) \frac{\partial \tilde{u}_k}{\partial x_k} \delta_{ji} - \frac{2}{3} \bar{\rho} \tilde{k} \delta_{ji}$$

Second Order Model

- Reynolds Stress Model

$$\overline{u_j'' u_i''}$$



Transport equation for $\tilde{\nu}$

$$\frac{\partial}{\partial t}(\bar{\rho}\tilde{\nu}) + \frac{\partial}{\partial x_i}(\bar{\rho}\tilde{\nu}u_i) = C_{b1}\rho\left[S + \frac{\tilde{\nu}}{\kappa^2 d^2}\left(1 - \frac{X}{1 + Xf_{v1}}\right)\right] + \frac{1}{\sigma_\nu}\left[\frac{\partial}{\partial x_j}\left((\mu + \rho\nu)\frac{\partial \nu}{\partial x_j}\right) + C_{b2}\rho\left(\frac{\partial \nu}{\partial x_j}\right)^2\right] - Y_\nu$$

Eddy viscosity $\mu_T = \rho\tilde{\nu}f_{v1}$

$$f_{v1} = \frac{X^3}{X^3 + C_{v1}^3} \quad Y_\nu = C_{\omega1}\rho g\left[\frac{1 + C_{\omega3}^6}{g^6 + C_{\omega3}^6}\right]^{1/6} \quad X = \frac{\tilde{\nu}}{\nu}$$

Damping function

Destruction of the viscosity

Normalized eddy viscosity



Turbulent kinetic energy

$$\frac{\partial}{\partial t}(\bar{\rho}\tilde{k}) + \frac{\partial}{\partial x_i}(\bar{\rho}\tilde{k}\tilde{u}_i) = \frac{\partial}{\partial x_j} \left[\left(\mu + \frac{\mu_t}{\sigma_t} \right) \frac{\partial \tilde{k}}{\partial x_j} \right] + \mu_T \tilde{S}^2 - \frac{1}{\bar{\rho}} g_i \frac{\mu_T}{\text{Pr}_T} \left(\frac{\partial \bar{\rho}}{\partial \tilde{T}} \right)_P \frac{\partial \tilde{T}}{\partial x_i} + \bar{\rho} \tilde{\varepsilon} - 2 \bar{\rho} \tilde{\varepsilon} M_t^2$$

Dissipation of the turbulent kinetic energy

$$\frac{\partial}{\partial t}(\bar{\rho}\tilde{\varepsilon}) + \frac{\partial}{\partial x_i}(\bar{\rho}\tilde{\varepsilon}\tilde{u}_i) = \frac{\partial}{\partial x_j} \left[\left(\mu + \frac{\mu_t}{\sigma_\varepsilon} \right) \frac{\partial \tilde{\varepsilon}}{\partial x_j} \right] + C_{1\varepsilon} \frac{\tilde{\varepsilon}}{\tilde{k}} \left(\mu_T \tilde{S}^2 + C_{3\varepsilon} \left(-\frac{1}{\bar{\rho}} g_i \frac{\mu_T}{\text{Pr}_T} \left(\frac{\partial \bar{\rho}}{\partial \tilde{T}} \right)_P \frac{\partial \tilde{T}}{\partial x_i} \right) \right) - C_{2\varepsilon} \bar{\rho} \frac{\tilde{\varepsilon}^2}{\tilde{k}}$$

Turbulent eddy viscosity

$$\mu_t = \bar{\rho} C_\mu \frac{\tilde{k}^2}{\tilde{\varepsilon}}$$

Turbulent Mach number

$$M_t^2 = \sqrt{\frac{\tilde{k}}{\gamma R \tilde{T}}}$$

Modulus of the mean
rate of strain tensor

$$\tilde{S} = \sqrt{2 \tilde{S}_{ij} \tilde{S}_{ij}}$$

Model coefficients

$C_{1\varepsilon}$	$C_{2\varepsilon}$	C_μ	σ_k	σ_ε
1.44	1.92	0.09	1.0	1.3



Turbulent kinetic energy

$$\frac{\partial}{\partial t}(\bar{\rho}\tilde{k}) + \frac{\partial}{\partial x_i}(\bar{\rho}\tilde{k}\tilde{u}_i) = \frac{\partial}{\partial x_j} \left[\alpha_k \mu_{eff} \frac{\partial \tilde{k}}{\partial x_j} \right] + \mu_T \tilde{S}^2 - \frac{1}{\bar{\rho}} g_i \frac{\mu_T}{Pr_T} \left(\frac{\partial \bar{\rho}}{\partial \tilde{T}} \right)_p \frac{\partial \tilde{T}}{\partial x_i} + \bar{\rho} \tilde{\varepsilon} - 2 \bar{\rho} \tilde{\varepsilon} M_i^2$$

Dissipation of the turbulent kinetic energy

$$\frac{\partial}{\partial t}(\bar{\rho}\tilde{\varepsilon}) + \frac{\partial}{\partial x_i}(\bar{\rho}\tilde{\varepsilon}\tilde{u}_i) = \frac{\partial}{\partial x_j} \left[\alpha_\varepsilon \mu_{eff} \frac{\partial \tilde{\varepsilon}}{\partial x_j} \right] + C_{1\varepsilon} \frac{\tilde{\varepsilon}}{\tilde{k}} \left(\mu_T \tilde{S}^2 + C_{3\varepsilon} \left(-\frac{1}{\bar{\rho}} g_i \frac{\mu_T}{Pr_T} \left(\frac{\partial \bar{\rho}}{\partial \tilde{T}} \right)_p \frac{\partial \tilde{T}}{\partial x_i} \right) \right) - C_{2\varepsilon} \bar{\rho} \frac{\tilde{\varepsilon}^2}{\tilde{k}} - R_\varepsilon$$

Additional destruction term

$$\tilde{\eta} \equiv \tilde{S} \tilde{k} / \tilde{\varepsilon}$$

$$R_\varepsilon = \frac{C_\mu \bar{\rho} \tilde{\eta}^3 (1 - \eta/\eta_0) \tilde{\varepsilon}^2}{1 + \beta \tilde{\eta}^3} \frac{1}{\tilde{k}}$$

$$\eta_0 = 4.38$$

$$\beta = 0.012$$

Model coefficients

$C_{1\varepsilon}$	$C_{2\varepsilon}$	C_μ	σ_k	σ_ε
1.44	1.92	0.09	0.72	0.72



Turbulent kinetic energy

$$\frac{\partial}{\partial t}(\bar{\rho}\tilde{k}) + \frac{\partial}{\partial x_i}(\bar{\rho}\tilde{k}\tilde{u}_j) = \frac{\partial}{\partial x_j} \left[\left(\mu + \frac{\mu_t}{\sigma_k} \right) \frac{\partial \tilde{k}}{\partial x_j} \right] + \mu_T \tilde{S}^2 - \frac{1}{\bar{\rho}} g_i \frac{\mu_T}{\text{Pr}_T} \left(\frac{\partial \bar{\rho}}{\partial \tilde{T}} \right)_P \frac{\partial \tilde{T}}{\partial x_i} - \bar{\rho}\tilde{\varepsilon} - 2\bar{\rho}\tilde{\varepsilon}M_i^2$$

Dissipation of the turbulent kinetic energy

$$\frac{\partial}{\partial t}(\bar{\rho}\tilde{\varepsilon}) + \frac{\partial}{\partial x_i}(\bar{\rho}\tilde{\varepsilon}\tilde{u}_j) = \frac{\partial}{\partial x_j} \left[\left(\mu + \frac{\mu_t}{\sigma_\varepsilon} \right) \frac{\partial \tilde{\varepsilon}}{\partial x_j} \right] + C_{1\varepsilon} \bar{\rho} \tilde{S} \tilde{\varepsilon} - C_2 \bar{\rho} \frac{\tilde{\varepsilon}^2}{\tilde{k} + \sqrt{\nu} \tilde{\varepsilon}} + C_{1\varepsilon} \frac{\tilde{\varepsilon}}{\tilde{k}} C_{3\varepsilon} \left(-\frac{1}{\bar{\rho}} g_i \frac{\mu_T}{\text{Pr}_T} \left(\frac{\partial \bar{\rho}}{\partial \tilde{T}} \right)_P \frac{\partial \tilde{T}}{\partial x_i} \right)$$

$$C_\mu = \frac{1}{A_0 + A_S \frac{\tilde{u}^* \tilde{k}}{\tilde{\varepsilon}}} \quad C_1 = \max \left[0.43, \frac{\tilde{\eta}}{\tilde{\eta} + 5} \right] \quad \tilde{\eta} = \tilde{S} \frac{\tilde{k}}{\tilde{\varepsilon}}$$

Model coefficients

$C_{1\varepsilon}$	C_2	σ_k	σ_ε
1.44	1.9	1.0	1.2



Turbulent kinetic energy

$$\frac{\partial}{\partial t}(\bar{\rho}\tilde{k}) + \frac{\partial}{\partial x_i}(\bar{\rho}\tilde{k}\tilde{u}_i) = \frac{\partial}{\partial x_j}\left[\Gamma_k \frac{\partial\tilde{k}}{\partial x_j}\right] + \mu_T \tilde{S}^2 - \bar{\rho}\beta^* f_{B*} \tilde{k} \tilde{\omega}$$

Specific dissipation rate

$$\frac{\partial}{\partial t}(\bar{\rho}\tilde{\omega}) + \frac{\partial}{\partial x_i}(\bar{\rho}\tilde{\omega}\tilde{u}_i) = \frac{\partial}{\partial x_j}\left[\Gamma_\omega \frac{\partial\tilde{\omega}}{\partial x_j}\right] + \alpha \frac{\tilde{\omega}}{\tilde{k}} \mu_t \tilde{S}^2 - \bar{\rho}\beta f_B \tilde{\omega}^2 + 2(1-F_1)\bar{\rho}\sigma_{\omega,2} \frac{1}{\tilde{\omega}} \frac{\partial\tilde{k}}{\partial x_j} \frac{\partial\tilde{\omega}}{\partial x_j}$$

Turbulent eddy viscosity $\mu_t = \alpha^* \frac{\rho k}{\omega}$

Effective diffusivities

$$\Gamma_k = \mu + \frac{\mu_t}{\sigma_k}$$

$$\Gamma_\omega = \mu + \frac{\mu_t}{\sigma_\omega}$$

Turbulent Prandtl numbers

$$\sigma_k = \frac{1}{F_1/\sigma_{k,1} + (1-F_1)/\sigma_{k,2}}$$

$$\sigma_\omega = \frac{1}{F_1/\sigma_{\omega,1} + (1-F_1)/\sigma_{\omega,2}}$$



Functions and Coefficients of dissipation of k

$$f_{\beta}^* = \begin{cases} 1 & \chi_k \leq 0 \\ \frac{1 + 680\chi_k^2}{1 + 400\chi_k^2} & \chi_k > 0 \end{cases} \quad \chi_k = \frac{1}{\omega^3} \frac{\partial k}{\partial x_j} \frac{\partial \omega}{\partial x_j}$$

$$\beta^* = \beta_i^* [1 + \zeta^* F(M_t)] \quad \beta_i^* = \beta_{\infty}^* \left(\frac{4/15 + (\text{Re}_t / R_B)^4}{1 + (\text{Re}_t / R_B)^4} \right)$$

$$\zeta^* = 1.5 \quad R_B = 8 \quad \beta_{\infty}^* = 0.09$$

Functions and Coefficients of dissipation of ω

$$f_{\beta} = \frac{1 + 70\chi_{\omega}}{1 + 80\chi_{\omega}} \quad \chi_{\omega} = \left| \frac{\Omega_{ij} \Omega_{ji} S_{ki}}{(\beta_{\infty}^* \omega)^3} \right| \quad \beta = \beta_i \left[1 - \frac{\beta_i^*}{\beta_i} \zeta^* F(M_t) \right]$$

Functions for calculation of turbulent viscosity

$$\alpha^* = \alpha_{\infty} \left(\frac{\alpha_0^* + \text{Re}_t / R_k}{1 + \text{Re}_t / R_k} \right) \quad \alpha = \frac{\alpha_{\infty}}{\alpha^*} \left(\frac{\alpha_0 + \text{Re}_t / R_{\omega}}{1 + \text{Re}_t / R_{\omega}} \right) \quad \text{Re}_t = \frac{\rho k}{\mu \omega}$$

$$R_k = 6 \quad \alpha_0^* = \beta_i / 3$$



Reynolds Stress Equation

$$\begin{aligned} \frac{\partial}{\partial t}(\bar{\rho}\tilde{\tau}_{ij}^R) + \frac{\partial}{\partial x_k}(\bar{\rho}\tilde{u}_k\tilde{\tau}_{ij}^R) = & -\frac{\partial}{\partial x_k}\left(\frac{\mu_t}{\sigma_t}\frac{\partial\tilde{\tau}_{ij}^R}{\partial x_k}\right) + \frac{\partial}{\partial x_k}\left[\mu\frac{\partial\tilde{\tau}_{ij}^R}{\partial x_k}\right] - \bar{\rho}\left(\tilde{\tau}_{ik}^R\frac{\partial\tilde{u}_j}{\partial x_k} + \tilde{\tau}_{jk}^R\frac{\partial\tilde{u}_i}{\partial x_k}\right) \\ & - \frac{\mu_t}{\bar{\rho}\text{Pr}_t}\left(g_i\frac{\partial\bar{\rho}}{\partial x_j} + g_j\frac{\partial\bar{\rho}}{\partial x_i}\right) + \phi_{ij} - \varepsilon_{ij} - 2\bar{\rho}\Omega_k\left(\tilde{\tau}_{jm}^R\tilde{\varepsilon}_{ikm} + \tilde{\tau}_{jm}^R\tilde{\varepsilon}_{jkm}\right) \end{aligned}$$

Turbulence viscosity

$$\mu_t = \bar{\rho}C_\mu\frac{\tilde{k}^2}{\tilde{\varepsilon}}$$

Dissipation tensor

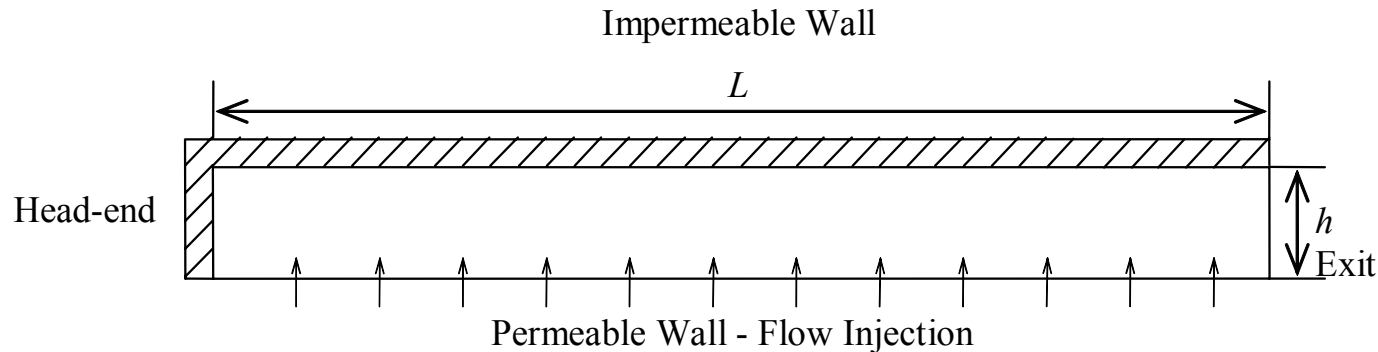
$$\varepsilon_{ij} = \frac{2}{3}\delta_{ij}(\bar{\rho}\varepsilon + Y_M)$$

Pressure strain term

$$\tilde{\Phi}_{ij} = \tilde{\Phi}_{ij,1} + \tilde{\Phi}_{ij,2} + \tilde{\Phi}_{ij,\omega}$$

$$\tilde{\Phi}_{ij,1} = -C_1\bar{\rho}\frac{\tilde{\varepsilon}}{\tilde{k}}\left[\tilde{\tau}_{ij}^R - \frac{2}{3}\delta_{ij}\tilde{k}\right] \quad \tilde{\Phi}_{ij,2} = -C_2\left[(\tilde{P}_{ij} + \tilde{F}_{ij} + \tilde{G}_{ij} - \tilde{C}_{ij}) - \frac{1}{3}\delta_{ij}(\tilde{P}_{kk} + \tilde{G}_{kk} - \tilde{C}_{kk})\right]$$

$$\tilde{\Phi}_{ij,\omega} = -C_1^0\frac{\tilde{\varepsilon}}{\tilde{k}}\left(\tilde{\tau}_{km}^R n_k n_m \delta_{ij} - \frac{3}{2}\tilde{\tau}_{ik}^R n_j n_k - \frac{3}{2}\tilde{\tau}_{jk}^R n_i n_k\right)\frac{\tilde{k}^{3/2}}{C_{\rho\delta l}} + C_2'\frac{\varepsilon}{\tilde{k}}\left(\tilde{\phi}_{km,2} n_k n_m \delta_{ij} - \frac{3}{2}\tilde{\phi}_{ik,2} n_j n_k - \frac{3}{2}\tilde{\phi}_{jk,2} n_i n_k\right)\frac{\tilde{k}^{3/2}}{C_{\rho\delta l}}$$



Schematics of the Vecla Facility

$$L = 0.581 \text{ m} \quad h = 0.0103 \text{ m}$$

Common Boundary Conditions

Injection Surface:

$$\dot{m} = 2.619 \text{ kg/m}^2 \text{ s}$$

$$T = 300 \text{ K}$$

Exit Surface:

$$P = 137400 \text{ Pa}$$

•Chaouat, B., 2000.

•Kourta, A., 2004.

Turbulence Model Specific Inlet Conditions

k- ϵ models $k = 0.0001 \text{ m}^2/\text{s}^2$

$$\epsilon = 0.001 \text{ m}^2/\text{s}^3$$

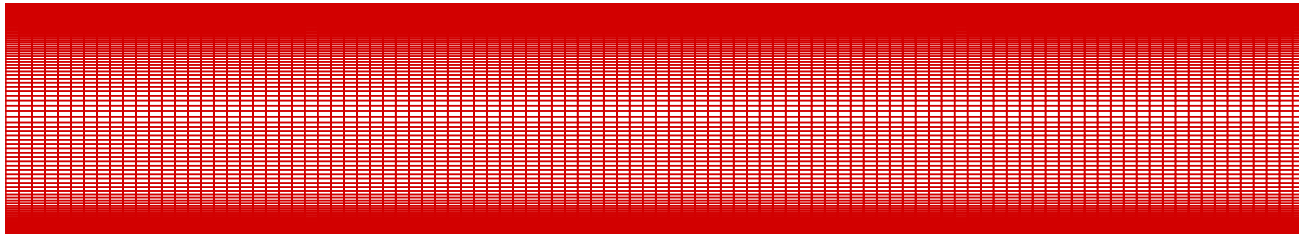
k- ω model $k = 0.0001 \text{ m}^2/\text{s}^2$

$$\omega = 0.4 \text{ s}^{-1}$$

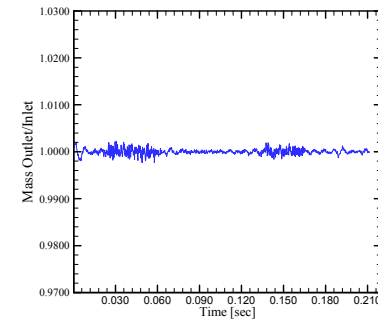
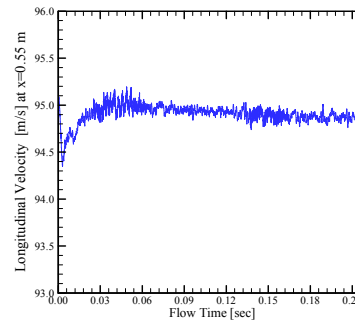
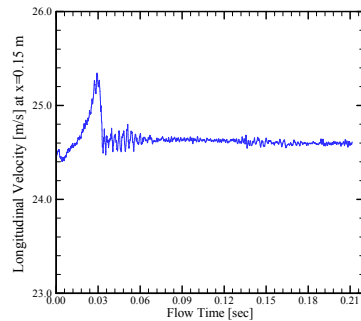
RSM $\overline{v''v''} = 0.092 \text{ m}^2/\text{s}^2$



Finite Volume Method (FLUENT)
Simple for Pressure velocity coupling
Second order upwind for remaining equations

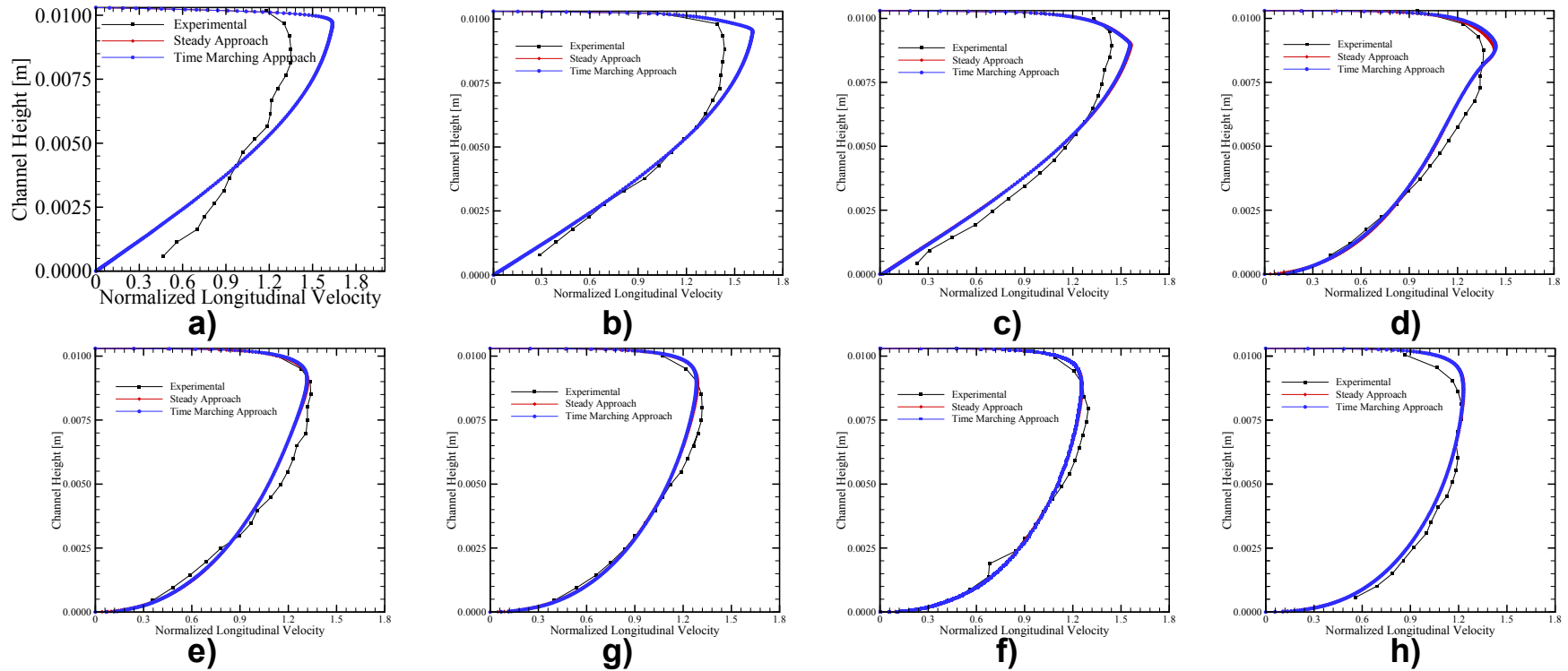


100 x 290 mesh points in x and y for steady calculations
100 x 242 mesh points in x and y for unsteady calculations



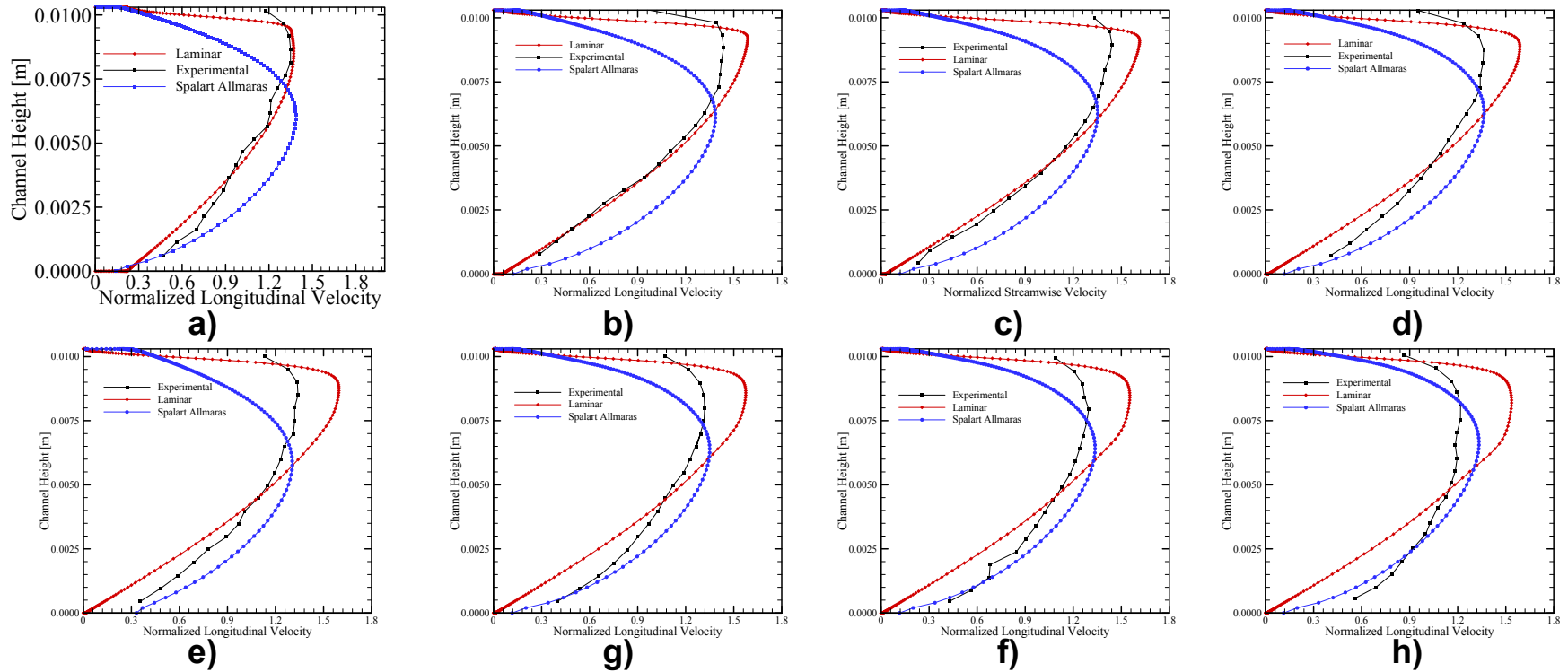
Time history for longitudinal velocity at sections a) 0.150 m, b) 0.55 m at mid height, and c) outlet to inlet mass flux ratio, obtained by time marching approach.

SST k- ω model has been used for time marching computations

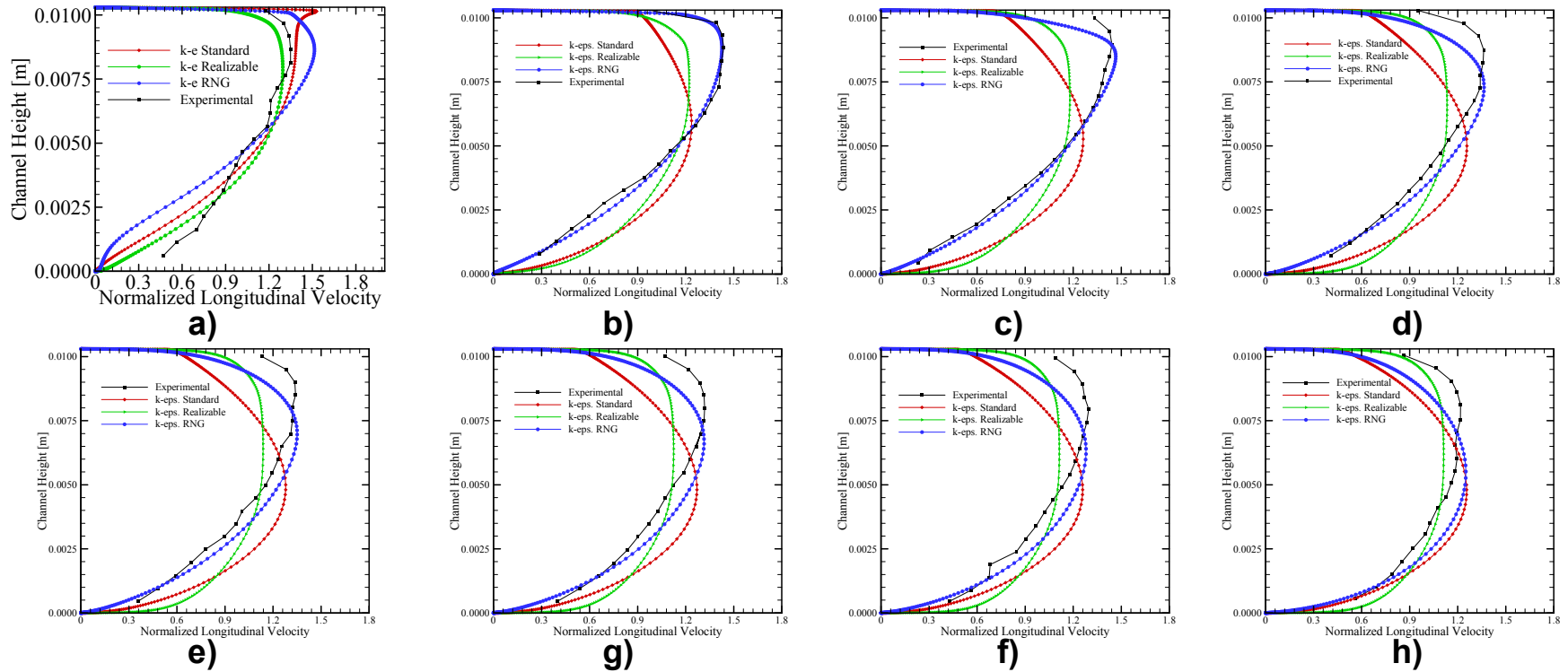


Comparison of the normalized longitudinal velocity distributions obtained by time marching and steady schemes at sections a) 0.031 m, b) 0.120 m., c) 0.220 m., d) 0.350 m., e) 0.400 m., f) 0.450 m., g) 0.500 m. and h) 0.570 m. for the coarse mesh.

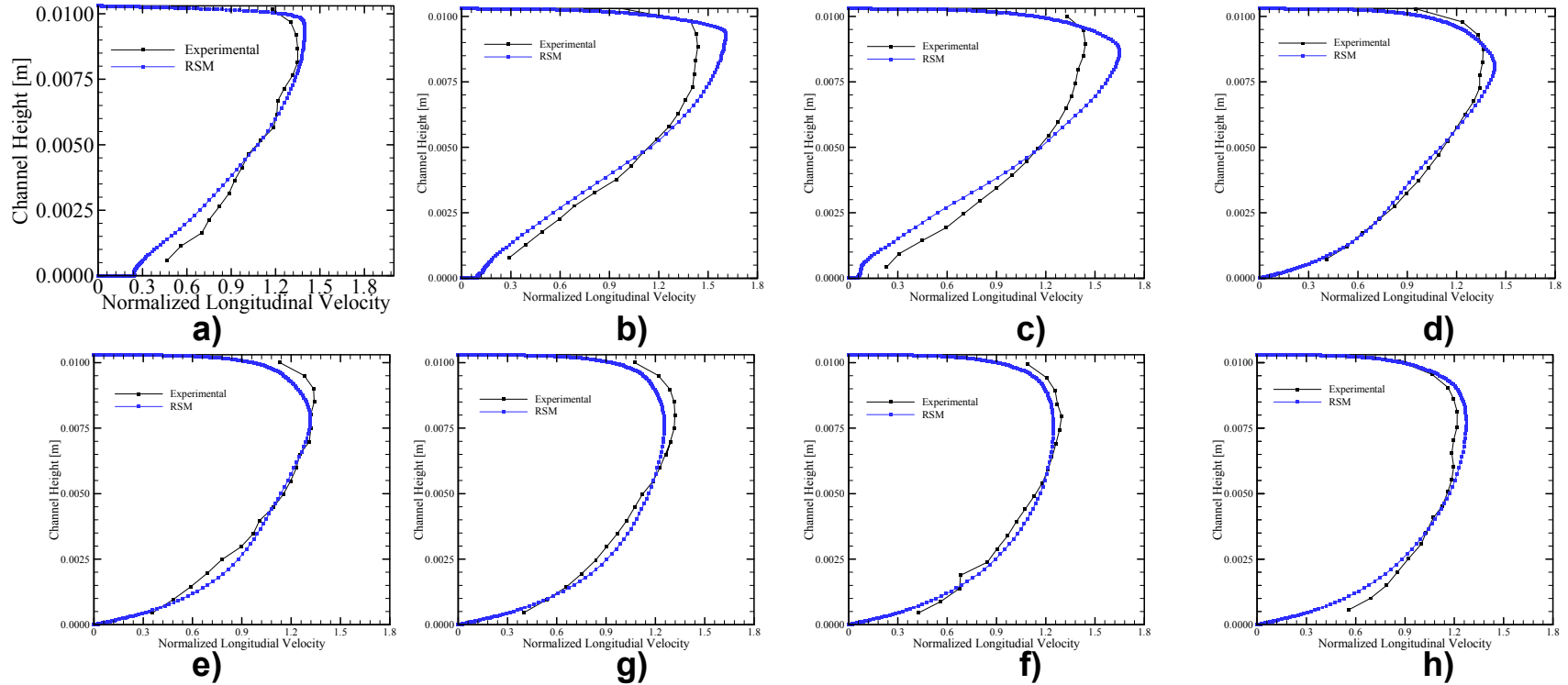
SST k- ω model has been used for comparison



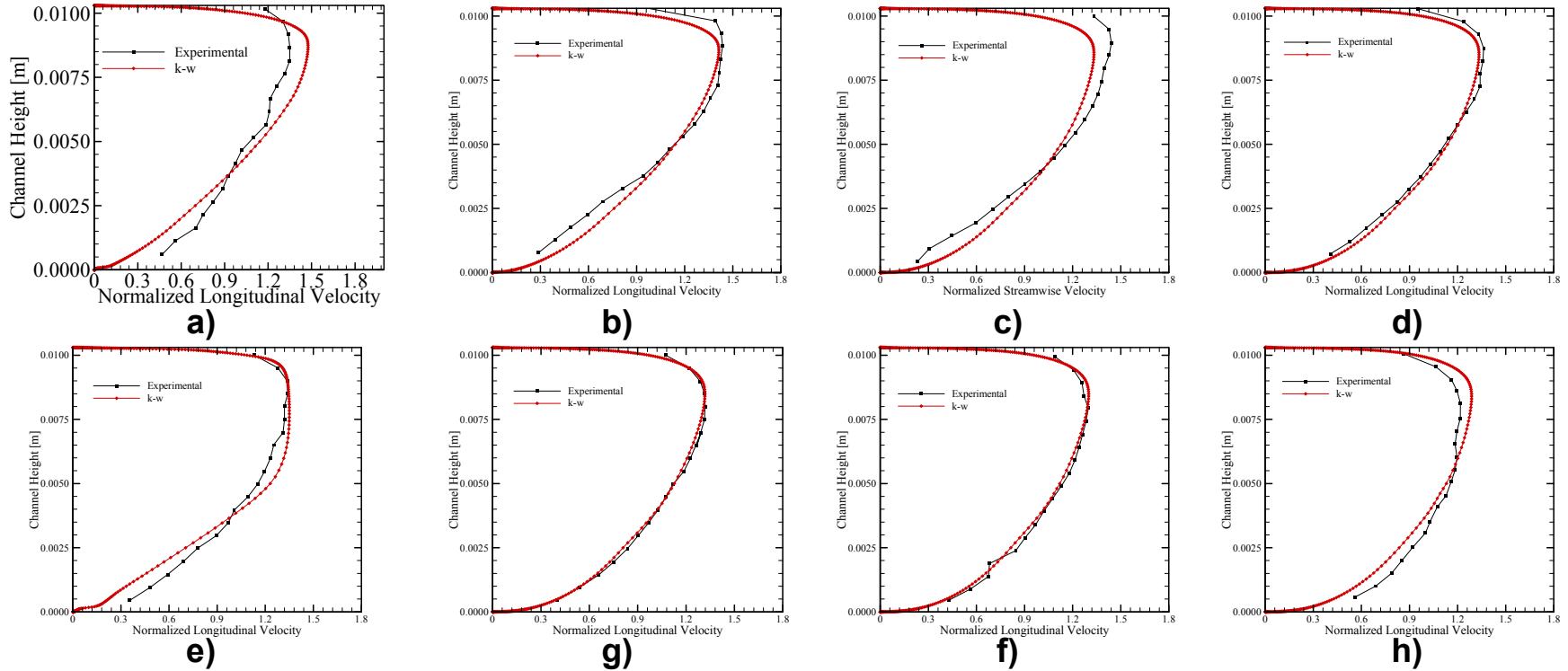
Normalized longitudinal velocity profiles obtained with the Laminar approach , the Spalart Allmaras turbulence closure model and from the experiment [3] at sections a) 0.031 m, b) 0.120 m., c) 0.220 m., d) 0.350 m., e)0.400 m., f) 0.450 m., g) 0.500 m. and h) 0.570 m. for the fine mesh.



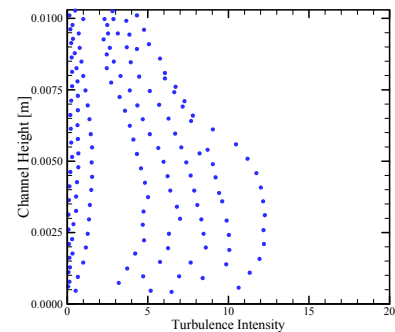
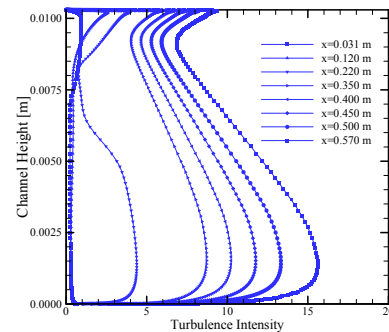
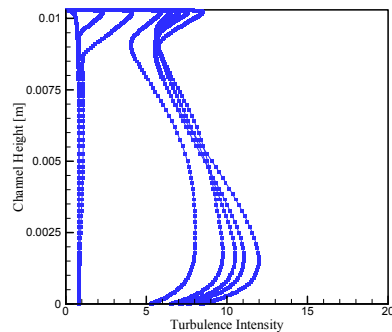
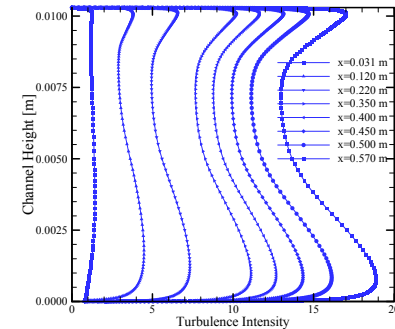
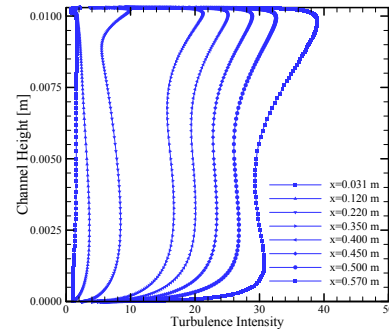
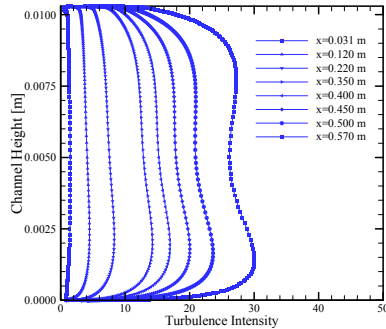
Normalized longitudinal velocity profiles obtained by the Standard $k-\varepsilon$, RNG $k-\varepsilon$, Realizable $k-\varepsilon$ turbulence closure models and from experiment at sections a) 0.031 m, b) 0.120 m., c) 0.220 m., d) 0.350 m., e) 0.400 m., f) 0.450 m., g) 0.500 m. and h) 0.570 m. for the fine mesh.



Normalized longitudinal velocity profiles obtained with the Reynolds Stress turbulence closure model and from experiment at sections a) 0.031 m, b) 0.120 m., c) 0.220 m., d) 0.350 m., e) 0.400 m., f) 0.450 m., g) 0.500 m. and h) 0.570 m. for the fine mesh.



Normalized longitudinal velocity profiles obtained by the SST $k-\omega$ turbulence closure model and from experiment at sections a) 0.031 m, b) 0.120 m., c) 0.220 m., d) 0.350 m., e) 0.400 m., f) 0.450 m., g) 0.500 m. and h) 0.570 m. for the fine mesh.



Turbulence intensity profiles obtained with the a) Standard $k-\varepsilon$, b) RNG $k-\varepsilon$, c) Realizable $k-\varepsilon$, d) Reynolds stress, e) SST $k-\omega$ turbulence closure models and f) from experiment, at eight sections



- k - ϵ based computations have not produced velocity and turbulence intensity profiles compatible with the experimental profiles, neither in the pre (laminar) nor post-transition (turbulent) sections.
- Computations based on the Reynolds Stress Model have predicted the normalized longitudinal velocity profiles well except for the laminar region, and turbulence intensity profiles are similar qualitatively as those from the experiments.
- SST k - ω turbulence closure model has yielded the longitudinal velocity profiles in a good agreement with the experiment [3]. Furthermore, accuracy of the turbulence intensity profiles was satisfactory compared with the results from the rest of the closure models.



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